## **Claims**

| 1  | 1. A gas purification system comprising:                                       |  |  |  |  |  |  |  |
|----|--|--|--|--|--|--|--|--|
| 2  | a reactor having a volume and a wall, the wall having an interior side         |  |  |  |  |  |  |  |
| 3  | and an exterior side, and a communicating portal therebetween for a mixed gas  |  |  |  |  |  |  |  |
| 4  | flow;  |  |  |  |  |  |  |  |
| 5  | a reaction catalyst coating in contact with the interior side of the wall;     |  |  |  |  |  |  |  |
| 6  | a gas selective membrane within the reactor volume, said gas                   |  |  |  |  |  |  |  |
| 7  | membrane in contact with the mixed gas flow and selectively passing a          |  |  |  |  |  |  |  |
| 8  | constituent gas of the mixed gas flow therethrough, whereby a raffinate of the |  |  |  |  |  |  |  |
| 9  | mixed gas flow is retained in contact with said membrane;                      |  |  |  |  |  |  |  |
| 10 | an outlet channel for removing said raffinate from contact with said           |  |  |  |  |  |  |  |
| 11 | selective membrane; and  |  |  |  |  |  |  |  |
| 12 | a passageway for the removal of the constituent gas from the interior of       |  |  |  |  |  |  |  |
| 13 | said reactor.  |  |  |  |  |  |  |  |
|    |  |  |  |  |  |  |  |  |
| 1  | 2. The gas purification system of claim 1 further comprising a                 |  |  |  |  |  |  |  |
| 2  | heater in thermal contact with said reactor.                                   |  |  |  |  |  |  |  |
|    |  |  |  |  |  |  |  |  |
| 1  | 3. The gas purification system of claim 1 further comprising a                 |  |  |  |  |  |  |  |
| 2  | space between the reaction catalyst coating and the membrane.                  |  |  |  |  |  |  |  |
|    |  |  |  |  |  |  |  |  |
| 1  | 4. The gas purification system of claim 3 wherein the space ranges             |  |  |  |  |  |  |  |

from 0.05 inch to 1.0 inch.

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| 1 | 5.            | The gas purification system of claim 3 wherein the space ranges |
|---|---------------|---|
| 2 | from 0.3 inch | to 0.6 inch.  |

- The gas purification system of claim 3 wherein the space 1 6. 2 comprises a flow distributor.
- The gas purification system of claim 6 wherein the flow 7. 1 distributor is selected from the group consisting of: packing, particulate, mesh 2 wire, wool, granule, pellet and fluidized catalyst. 3
- The gas purification system of claim 6 wherein the flow 1 8. distributor is a multichannel monolith. 2
- The gas purification system of claim 8 wherein the multichannel 9. monolith has channels ranging in diameter from 10 micrometers to 1 2 3 millimeter.
- The gas purification system of claim 8 wherein the multichannel 10. 1 monolith has channels ranging in diameter from 50 micrometers to 500 2 3 micrometers.
- The gas purification system of claim 8 wherein the monolith 1 11. 2 channels are coated.

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| 1 | 12.             | The   | gas  | purification   | system   | of | claim | 8 | wherein | the | monolith |
|---|-----------------|-------|------|----------------|----------|----|-------|---|---------|-----|----------|
| 2 | channels are co | oated | with | n a reaction c | atalyst. |    |       |   |         |     |          |

- The gas purification system of claim 8 wherein the monolith 1 13. 2 channels are coated with a selective membrane.
- 1 14. The gas purification system of claim 8 wherein the monolith is 2 bonded to the reactor wall such that heat is conducted from the wall exterior to the wall interior. 3
- 15. The gas purification system of claim 8 wherein the heating 2 means comprises a combustion catalyst.
- 16. The gas purification system of claim 15 wherein the combustion 2 catalyst is on the exterior wall of the reactor.
- 17. The gas purification system of claim 15 wherein the combustion 1 2 catalyst is on the exterior wall of a feed tube.
- The gas purification system of claim 1 further comprising a flow 1 18. 2 disruptor.

- 1 19. The gas purification system of claim 18 wherein the flow disruptor is selected from the group consisting of: a bump, a protrusion, a baffle and a helical tube.
- 1 20. The gas purification system of claim 2 wherein the heating 2 means comprises a sweep gas.
- 1 21. The gas purification system of claim 20 wherein the sweep gas 2 is inert.
- 1 22. The gas purification system of claim 21 wherein the sweep gas 2 is steam.
- 1 23. The gas purification system of claim 1 further comprising 2 partial pressure decreasing means.
- 1 24. The gas purification system of claim 23 wherein the partial pressure decreasing means is sweep gas flow.
- 1 25. The gas purification system of claim 1 further comprising feed 2 liquid compression means.

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plurality of the membranes.

| 1 | 26.      | The gas purification system of claim 1 wherein the membrane is |
|---|----------|--|
| 2 | tubular. |  |
|   |          |  |
| 1 | 27.      | The gas purification system of claim 1 further comprising a    |

- 1 28. The gas purification system of claim 1 wherein the membrane is
- 2 hydrogen selective and the constituent gas is hydrogen.
- 1 29. The gas purification system of claim 1 wherein the catalyst coating comprises a methanol reforming catalyst.
- 1 30. The gas purification system of claim 1 wherein the catalyst coating comprises an ammonia cracking catalyst.
- 1 31. The gas purification system of claim 1 wherein heat is provided 2 by catalytic combustion.
- 1 32. The gas purification system of claim 1 wherein said reactor 2 further comprises a heat transfer fin on the exterior surface thereof.
  - 33. A gas purification system comprising:

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| 2  | a reactor operating above room temperature having a volume and a                 |  |  |  |  |  |  |
|----|--|--|--|--|--|--|--|
| 3  | wall, the wall having an interior side and an exterior side, and a communicating |  |  |  |  |  |  |
| 4  | portal therebetween for a mixed gas flow;  |  |  |  |  |  |  |
| 5  | a gas selective membrane within the reactor volume, said gas                     |  |  |  |  |  |  |
| 6  | membrane in contact with the mixed gas flow and selectively passing a            |  |  |  |  |  |  |
| 7  | constituent gas of the mixed gas flow therethrough, whereby a raffinate of the   |  |  |  |  |  |  |
| 8  | mixed gas flow is retained in contact with said membrane;                        |  |  |  |  |  |  |
| 9  | an outlet channel for removing said raffinate from contact with said             |  |  |  |  |  |  |
| 10 | selective membrane;  |  |  |  |  |  |  |
| 11 | a catalyst in contact with the exterior side of said reactor that induces an     |  |  |  |  |  |  |
| 12 | exothermic combustion reaction with the raffinate; and                           |  |  |  |  |  |  |
| 13 | a passageway for the removal of the constituent gas from the interior of         |  |  |  |  |  |  |
| 14 | said reactor.  |  |  |  |  |  |  |
|    |  |  |  |  |  |  |  |
| 1  | 34. The gas purification system of claim 33 further comprising an                |  |  |  |  |  |  |
| 2  | insulating jacket surrounding said reactor, the jacket having an oxygen          |  |  |  |  |  |  |
| 3  | containing gas flowing therethrough.   |  |  |  |  |  |  |
|    |  |  |  |  |  |  |  |
| 1  | 35. The gas purification system of claim 33 further comprising a                 |  |  |  |  |  |  |
| 2  | plurality of the membranes.  |  |  |  |  |  |  |
|    |  |  |  |  |  |  |  |

36. The gas purification system of claim 33 wherein the membrane is hydrogen selective and the constituent gas is hydrogen.

- 1 37. The gas purification system of claim 33 wherein the membrane
- 2 is a tube membrane.